# LOOKING INTO THE CRYSTAL BALL WHERE IS THE WATER AND WASTEWATER INDUSTRY HEADED?



2019 Central West Texas Regional School

Joshua L. Berryhill, P.E. Enprotec / Hibbs & Todd, Inc. (eHT)



# **Presentation Topics**

#### Water Discussion

- Current Major Water Regulations
- Anticipated Updates to Current Water Rules
- Anticipated New Water Rules Coming
- Current Water Treatment Technology Options
- Future Water Tech

#### > Wastewater Discussion

- Current Major Wastewater Regulations
- Anticipated Updates to Current Wastewater Rules
- Anticipated New Wastewater Rules Coming
- Current Wastewater Treatment Technology Options
- Future Wastewater Tech

# **Current Major Water Regulations**

- LT2 Long Term Stage 2 Enhanced Surface Water Treatment Rule
  - <= 0.3 Nephelometric Turbidity Units (NTU) 95% of the time
  - <= 1.0 NTU 100% of the time</p>

- DB2 Stage 2 Disinfectants and Disinfection Byproducts Rule
  - Locational Running Annual Average (LRAA) for Total Trihalomethanes (TTHM) of 80 parts per billion (ppb)
  - LRAA for Haloacetic Acids (HAA5) of 60 ppb

#### ➤ LT3?

- Long Term 3 Enhanced Surface Water Treatment Rule
- Turbidity is an indirect indicator of potential for pathogen exposure risk – SWTR focuses on reduction of finished water turbidity
- Anticipated within the next 5-10 years

## History of ESWTR

- Original SWTR 1989
  - Interim Enhanced SWTR 1998
    - Long Term 1 ESWTR 2002
      - » Long Term 2 ESWTR 2006
        - Long Term 3....?

- > Why is LT3 a concern?
  - Current filter requirements
    - < 0.3 Nephelometric Turbidity Units (NTU) 95% of the time
    - < 1.0 NTU 100% of the time
    - These limits can be met by 99+% of the water utilities in Texas
  - Original version of LT2 proposed by EPA
    - < 0.1 NTU 95% of the time
    - < 0.3 NTU 100% of the time
    - These lower limits can only be met consistently with the use of membrane filtration technology

## ≻ DB3?

- Stage 3 Disinfectants and Disinfection Byproducts Rule
- Disinfection of water can create carcinogenic compounds
  Focus is on reducing the potential for carcinogen exposure risk
- Anticipated within the next 2-3 years

## ➢ History of DBP

- Original DBP Rule 1998
  - Stage 1 DBP Rule Revisions 2001
    - Stage 2 DBP Rule 2006
      - Stage 3....?

- ➢ Why is DB3 a concern?
  - Current DBP requirements
    - < 80 parts per billion (ppb) Total Trihalomethanes (TTHM)</li>
    - < 60 ppb Haloacetic Acids (HAA5)</li>
    - These limits can be met by most of the water utilities in Texas, with most utilities switching from free chlorine to chloramine use
  - Growing concerns about chloramination byproducts (not currently regulated...yet)
  - Potential changes in the future (if still focusing on just free chlorine based DBPs)
    - < 40-60 ppb TTHM
    - < 30-40 ppb HAA5
    - These limits will be difficult to meet consistently without major treatment changes

- Perchlorate
- > Strontium
- PFAS
- > NDMA
- Additional TTHMs
- Additional HAA5s

#### Perchlorate

- Active ingredient in many different types of rocket booster fuel, explosives, ordinance – previously thought to be focused around military bases, now found worldwide
- Concern as potential carcinogen
- Strontium
  - Commonly found in brackish water supplies
  - Concern on impacts to growth and development of children

#### PFAS – Per- and Polyfluoroalkyl Substances

- A "wonder chemical" used since 1940, primarily used in cookware – it does not break down naturally, so is now found worldwide
- Concern as potential carcinogen, both with mutagenic and teratogenic impacts (cancer for you, impacts to your children and grandchildren)

#### NDMA – N-Nitrosodimethylamine

- Found in some industrial processes, most commonly produced through chloramination of drinking water and wastewater
- Concern as potential carcinogen

#### Additional TTHMs

- Current regulations are based on free chlorine formed TTHMs Additional TTHMs are formed through chloramination as well, just not currently regulated
- Concern as potential carcinogen

#### Additional HAA5s

- Current regulations are based on free chlorine formed HAA5 Additional HAA5 are formed through chloramination as well, just not currently regulated
- Concern as potential carcinogen

- Meet Lower Turbidity Requirements
  - Implement membrane filtration technology, either in the form of microfiltration or ultrafiltration
  - Can operate in pressure or submerged vacuum mode
  - Multiple proven systems in Texas, with the oldest almost 20 years old







#### Meet Reduced DBP Limits

- Can treat before disinfection, after disinfection, or both
- Before Disinfection
  - Reduce formation potential before reacting with chlorine
  - Reduce TOC with enhanced coagulation, GAC, chlorine dioxide, ozone, peroxide, permanganate, UV-AOP, RO, NF
- After Disinfection
  - "Strip" formed DBPs from finished water
  - Clearwell mixing, air addition, forced ventilation

#### Meet Strontium Limit

- Implement desalination type technology
  - Reverse Osmosis (RO)
  - Nanofiltration (NF)
  - Electrodialysis (ED)
  - Electrodialysis Reversal (EDR)
  - Electrodistillation (EDI)





#### Meet PFAS Limit

- Implement RO or GAC
  - Reverse Osmosis Effective large-scale, and limited effectiveness for POU units
  - Granular Activated Carbon Effective large-scale, short operating life for POU units





- Meet NDMA or Tightened TTHM/HAA5 Limits
  - Need to focus on treatment prior to disinfection
    - Reduce formation potential before reacting with chlorine
      - Need to consider alternate disinfection options no more chlorine?
    - Reduce TOC with enhanced coagulation, GAC, chlorine dioxide, ozone, peroxide, permanganate, UV-AOP, RO, NF

## **Future Water Tech**

#### Upcoming Technologies

- Electrocoagulation
  - Can minimize or eliminate the need for coagulant while completing enhanced coagulation of TOC
- Forward Osmosis
  - Performance is similar to RO, but at a fraction of energy use
  - Currently in prototype testing in UAE
- Ozone/BAF
  - Ozonation combined with Biologically Active Filters
  - Concerns about Bromate formation
  - Current being tested in Dallas, TX

## **Wastewater Discussion**

# **Current Major Wastewater Regulations**

- > What are typical current permit limits in Texas?
  - Natural Treatment (Lagoon) Systems
    - BOD 30 mg/L
    - TSS 90mg/L
  - Mechanical Treatment WWTPs
    - BOD (or cBOD) 5-15 mg/L
    - TSS 7-15 mg/L
    - NH<sub>3</sub> 2-3 mg/L
  - Reuse
    - Type II Non-Potable Reuse
      - BOD (or cBOD) 20 mg/L
    - Type I Non-Potable Reuse
      - BOD (or cBOD) 5 mg/L
      - Turbidity 3 NTU

- What changes are anticipated to current permit limits in Texas?
  - Changes are site specific to a given receiving stream, but changes are occurring throughout Texas
  - BOD or cBOD
    - 5-15 mg/L -> 5-7 mg/L
  - TSS
    - 7-15 mg/L -> 5-7 mg/L
  - Ammonia (NH<sub>3</sub>)
    - 2-3 mg/L -> 1-2 mg/L
  - E. Coli
    - 126 CFU / 100 ml -> 63 CFU / 100 ml

> What changes may be coming to permitting?

- Numeric Nutrient Criteria Development Plan
  - <u>WAS</u> anticipated to become active in <u>2016</u>
  - Intended to evaluate WWTPs for the potential of adding a total phosphorus (TP) and/or total nitrogen (TN) limit to permits
  - Triggers for further evaluation:
    - WWTP permit rating >= 0.5 MGD
    - TP in effluent >= 3.5 mg/L
    - TN in effluent >= 15 mg/L (primarily in coastal areas)
    - Discharge stream segment is impaired for anything



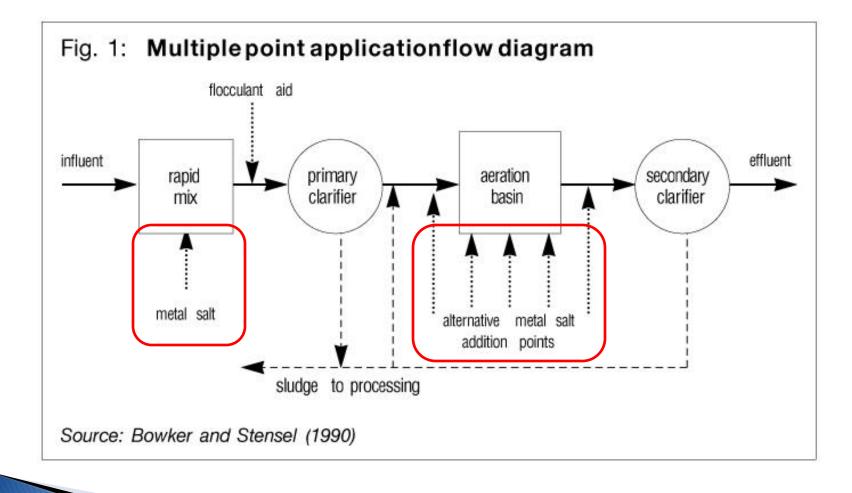
- > What if I get a nutrient limit added to my permit?
  - Total Nitrogen
    - Need to start planning for adding a nitrogen removal step
      - Biological Removal of Ammonia/Nitrate/Nitrite
  - Total Phosphorus
    - Need to start planning for adding a phosphorus removal step
      - Chemical Removal?
      - Biological Removal?
      - Filtration Removal?

- Advanced Nitrogen Reduction
  - Biological Removal
    - Ammonia (NH<sub>3</sub>)
      - Removal via nitrification step in aerobic selector zone, conversion to nitrate  $(NO_3)$
    - Nitrate (NO<sub>3</sub>) and Nitrite (NO<sub>2</sub>)
      - Addition of an anoxic (zero free dissolved oxygen) selector zone upstream of the aerobic selector zone

$$2NO_{3}^{-} \rightarrow 2N_{2}^{0} \xrightarrow{\uparrow} 2NO \rightarrow N_{2}O \rightarrow N_{2}$$
[2]

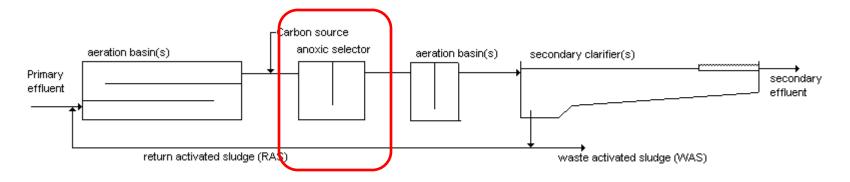
- Phosphorus Reduction
  - Chemical Removal
    - Can remove orthophosphate (PO<sub>4</sub>, HPO<sub>4</sub>, H<sub>2</sub>PO<sub>4</sub>) via chemical bonding and precipitation
    - Addition of a metal salt such as alum (aluminum sulfate) or ferric (ferric sulfate) can bond with phosphorus
    - Can typically remove down to 0.5-1.0 mg/L
    - AI +  $PO_4 => AIPO_4$ 
      - Works best at a pH range of 5-7
      - Potential nitrification impacts
    - Fe +  $PO_4 => FePO_4$ 
      - Works best at a pH range of 6.5-7.5

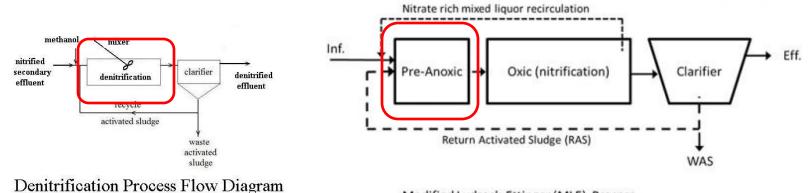




How can phosphorus be removed at a WWTP?

- Biological Removal
  - Orthophosphate
    - Biomass does not readily absorb orthophosphate, the orthophosphate must be converted to polyphosphate for uptake
    - Conversion occurs via breakdown in an anaerobic selector zone (no presence of oxygen), along with the production of volatile fatty acids (VFAs)
  - Polyphosphate
    - Biomass in the aerobic selector zone called phosphorus accumulating organisms (PAOs) absorb excess phosphorus while consuming VFAs
  - Can typically remove phosphorus down to 0.5 mg/L

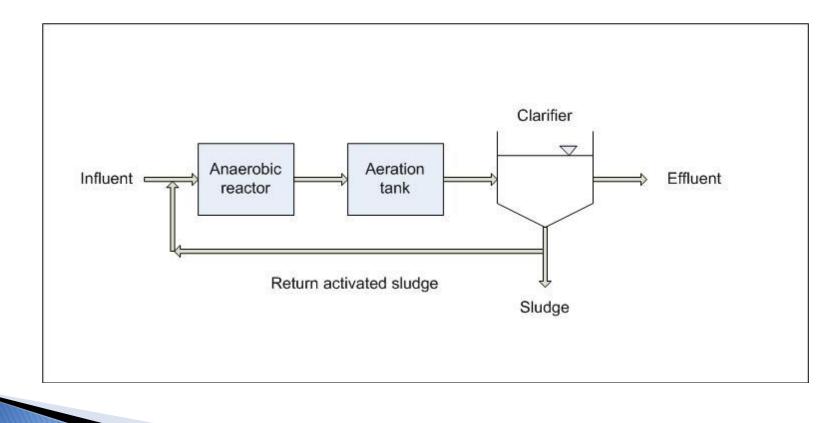




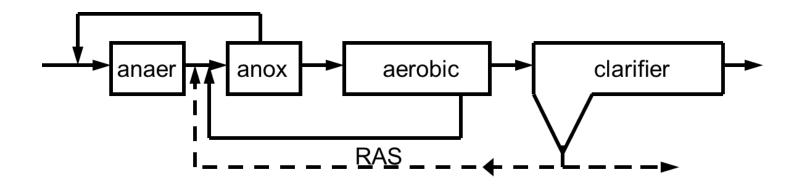
Modified Ludzack-Ettinger (MLE) Process

27

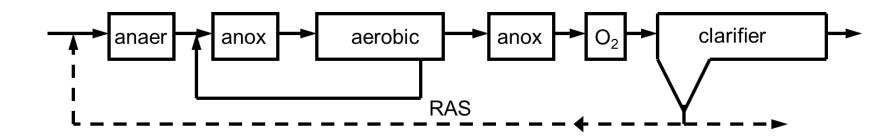
## • Anaerobic-Oxic (AO) Process

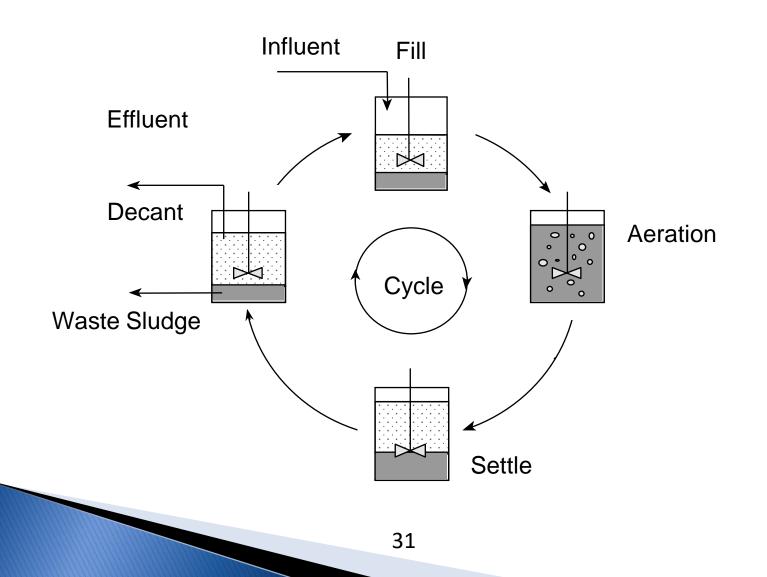


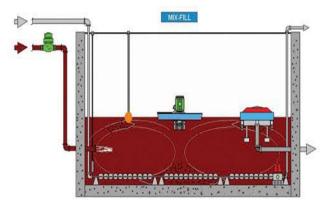
## University of Capetown (UCT) Process

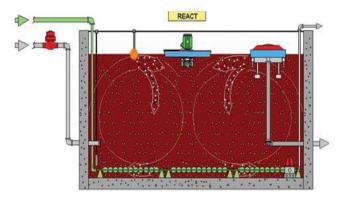


Bardenpho Process



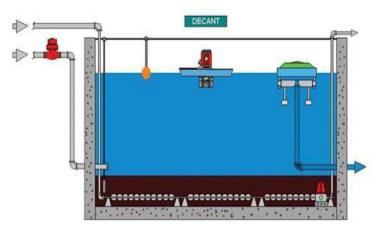




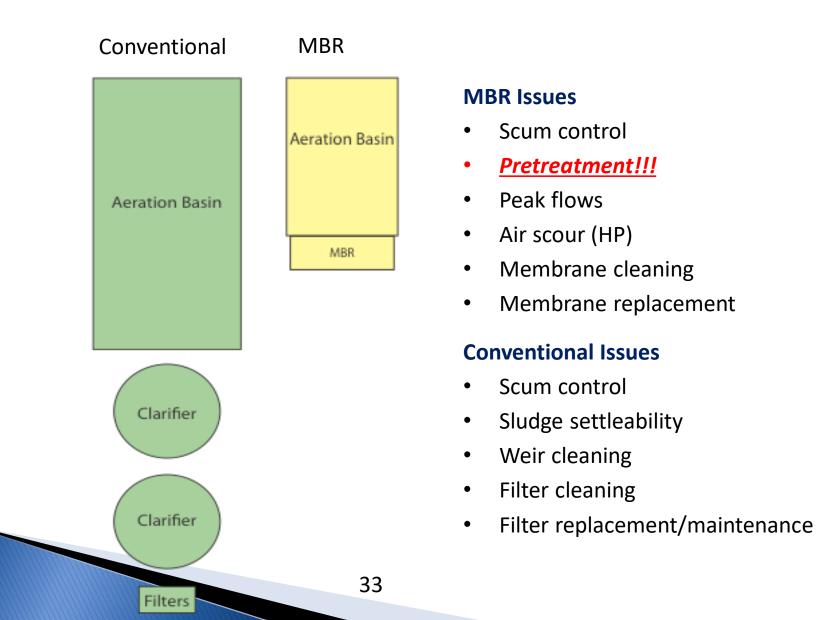


FILL





SETTLE/DECANT



#### ➤ MBR System Type – Hollow Fiber

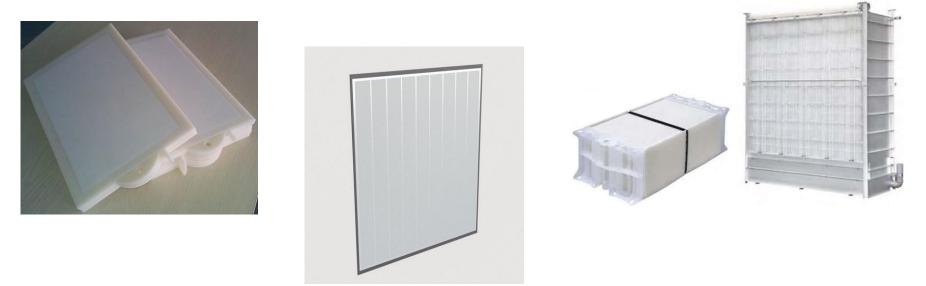








#### ➤ MBR System Type – Flat Sheet

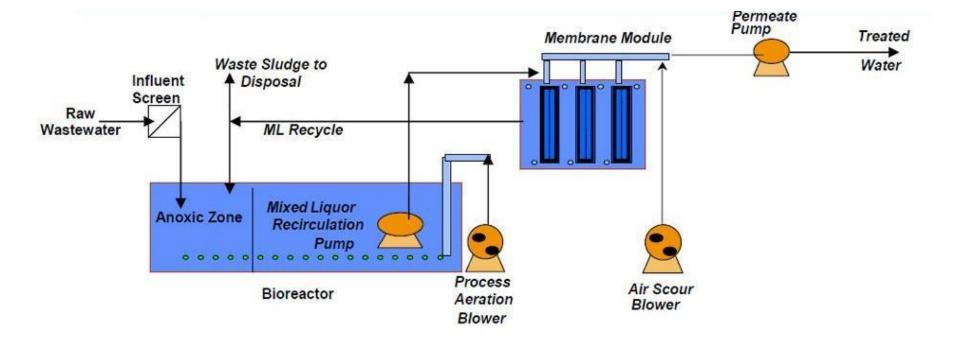






### **Advanced Treatment Technologies - MBR**

### Historical Custom MBR Design

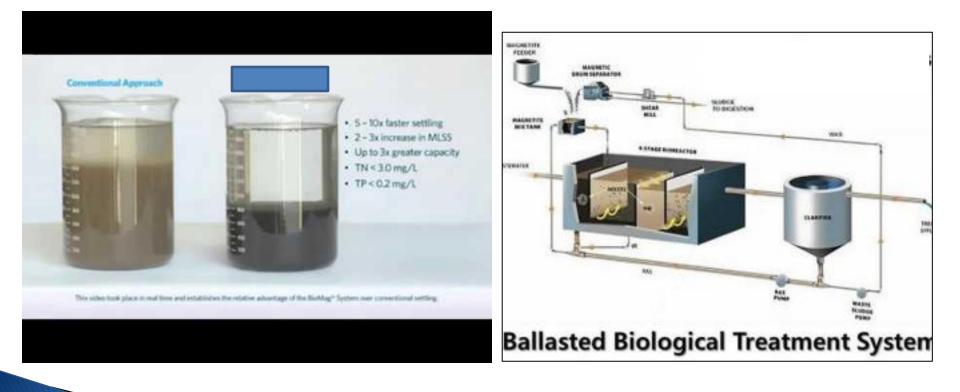


### Ceramic MBR Systems

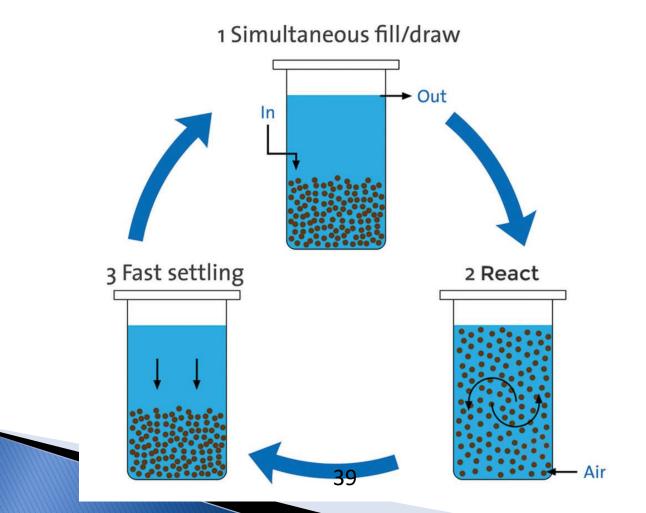




## Magnetite Ballasted Biological Treatment System

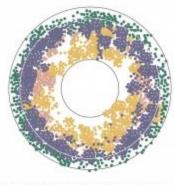


## Granular Biological Treatment System



### Granular Biological Treatment System

What is Aerobic Granular Sludge? Aerobic granular sludge represents an emerging approach for intensifying biological treatment at WRRFs in order to do more with less.



These granules allow for simultaneous removal of carbon, nitrogen, and phosphorus. C P

40

At the heart of the process is the development of fast settling aggregates of bacterial communities (granules).

Fast settling granules also allow WRRFs to separate the solids and liquids more effectively than with conventional activated sludge. Improvements to settling associated with granular sludge are generally reflected in low sludge volume index measurements (SVI). State of the Industry Early adopters are already seeing

these substantial benefits over an activated sludge process:



Smaller footprint when compared with activated sludge



Lower construction and operational costs



Energy savings

## **Questions?**

# Thank you for your time!

For additional information, please contact Joshua Berryhill at joshua.berryhill@e-ht.com

Joshua Berryhill, P.E. Enprotec / Hibbs & Todd, Inc. (eHT)

