

# When Membrane 1.0 isn't enough, time to change to Membrane 2.0!

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**South Central Membrane Association**  
2021 Virtual Conference

**Solving Membrane Operation &  
Management Challenges**

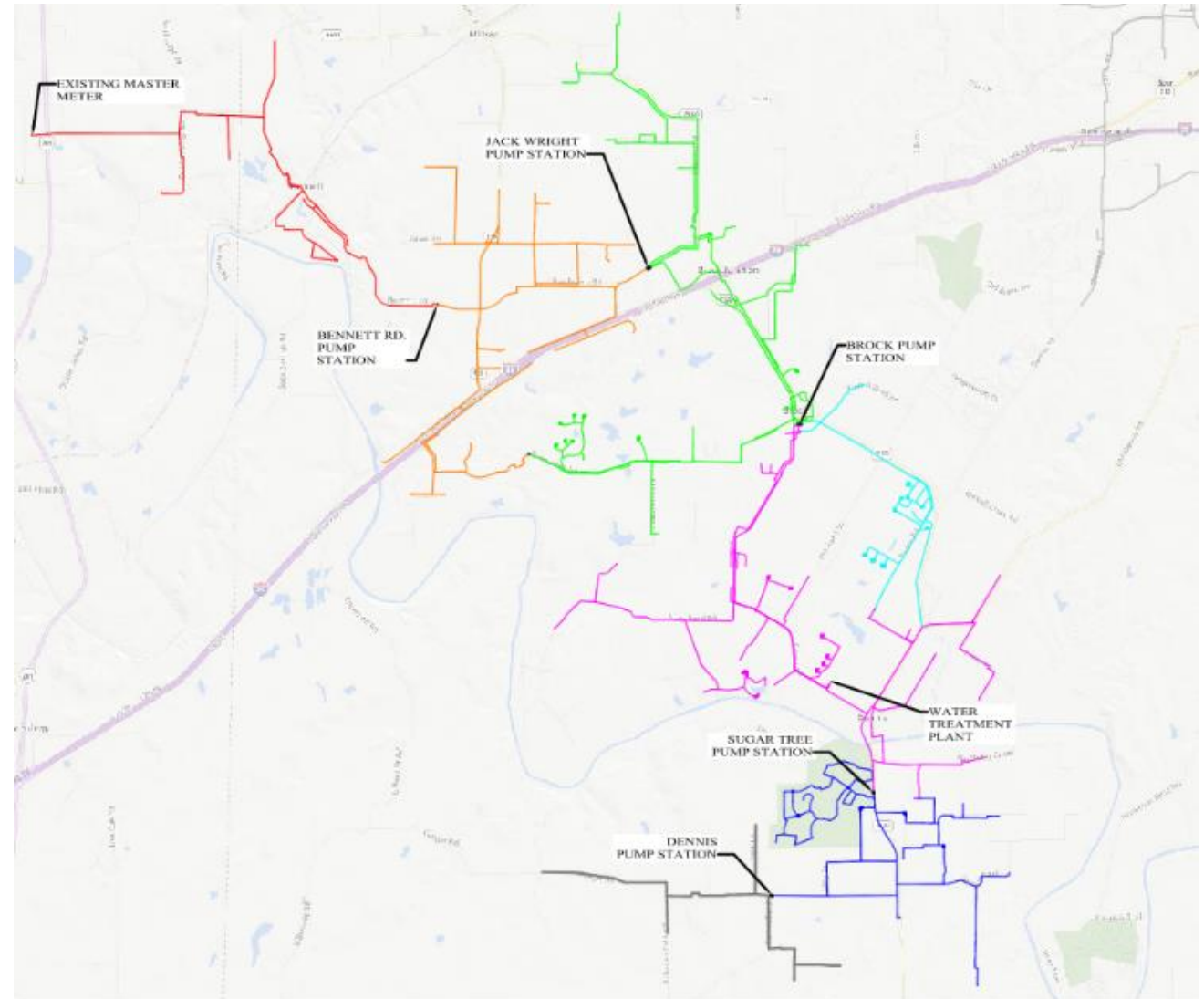
August 25th - 26th

# Presentation Topics

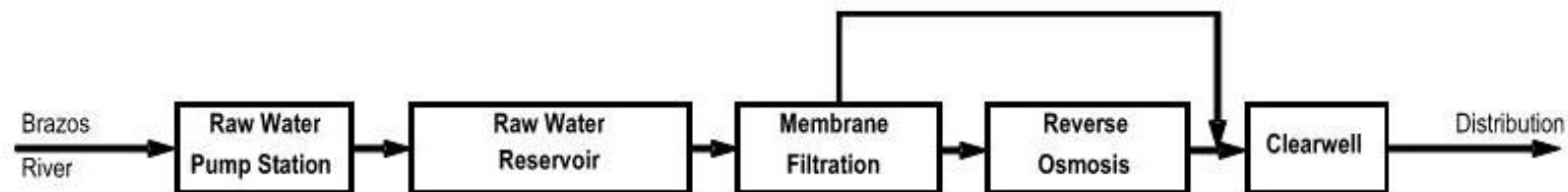
- Background on Parker County SUD Water System
- Historical Treatment Challenges
- Corrective Actions Considered
- Advanced Membrane Filter Pilot Testing Observations
- Project Path Forward and Next Steps
- Final Thoughts

# Background on Parker County SUD Water System

- Rural Water System
- Currently approx. 1,900 connections
- Surface Water (Brazos River) and Groundwater (Upper Trinity)
- 1.0 MGD Treated Surface Water
- 0.4 MGD Wholesale Water Purchase (Mineral Wells)

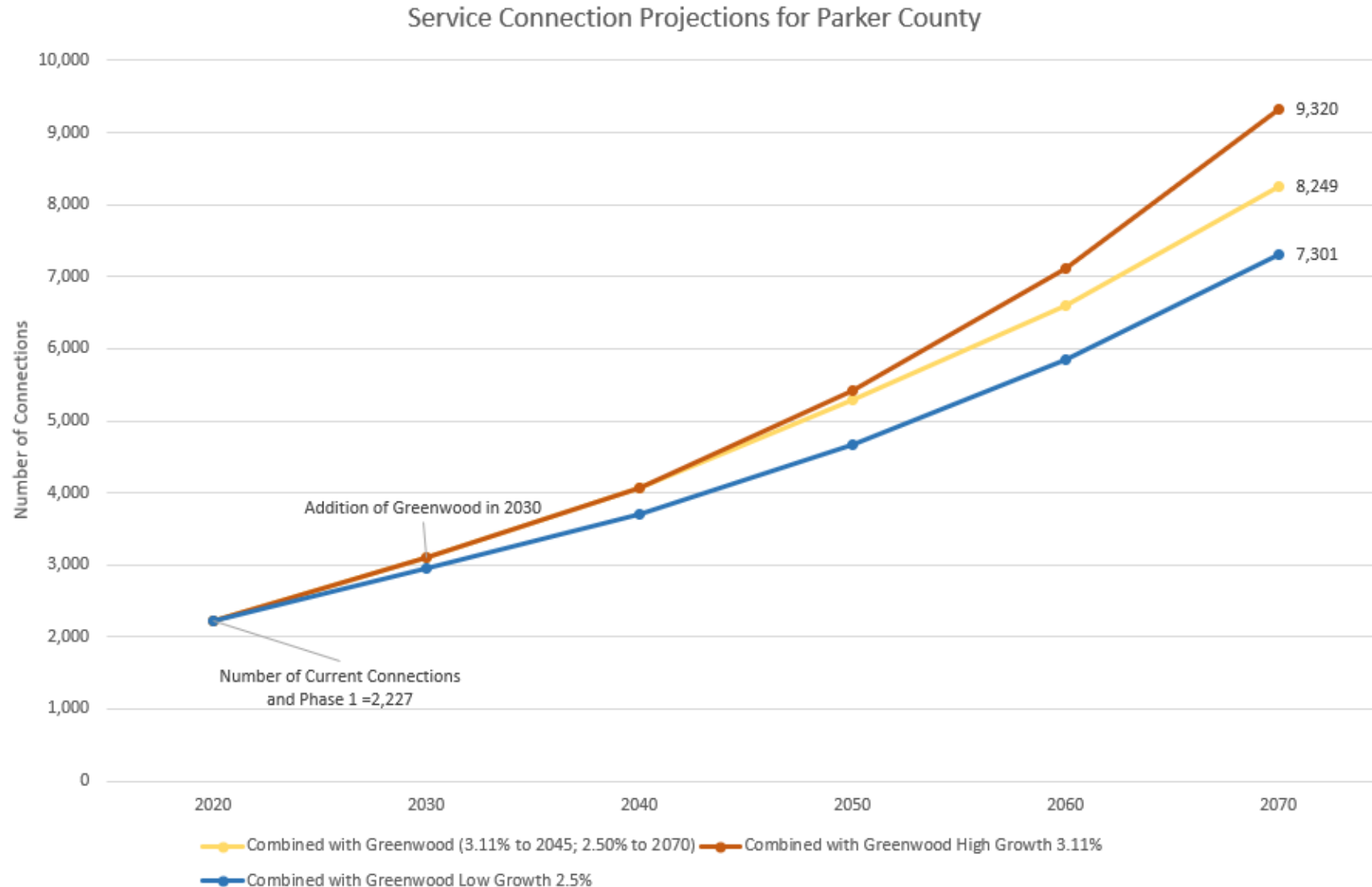


# Background on Parker County SUD Water System





# Background on Parker County SUD Water System



# Historical Treatment Challenges

Only Permeate  
Storage to Complete  
1 Low or High pH  
Clean for 1 Train

Flux  
Design – 52 gfd  
Actual - <25 gfd

No strong oxidant  
pretreatment

Significant Mn  
Concentration  
Due to Internal  
Plant Recycle

Paper Capacity –  
1.0 MGD  
Actual Capacity –  
0.6 MGD

No coagulant or  
other  
pretreatment

2 MF trains  
1 RO train

# Corrective Actions Considered

## Improve Pretreatment

- Implement strong oxidant in raw water (ClO<sub>2</sub>, KMnO<sub>4</sub>, H<sub>2</sub>O<sub>2</sub>)
- Implement coagulant (iron- or aluminum-based coagulant)
- Implement clarification pretreatment

## Improve Operational Flexibility

- Install 2<sup>nd</sup> RO train
- Install additional RO permeate storage
- Maintain total chlorine through RO to reduce biofouling

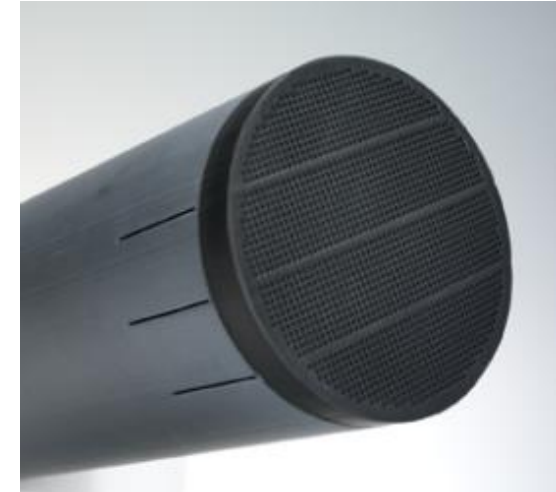
## Increase MF Capacity

- Increase sustained flux in existing MF trains
- Install additional MF trains
- Test performance of more advanced MF technology

# Corrective Actions Considered

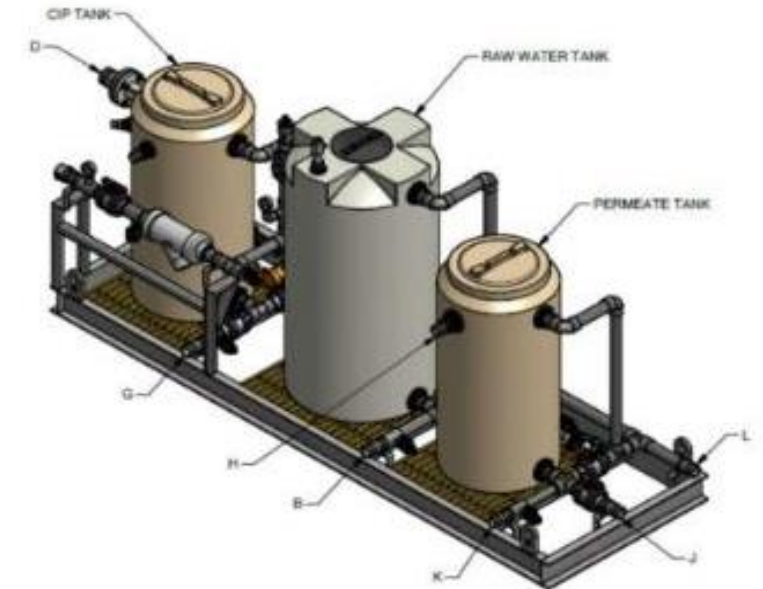
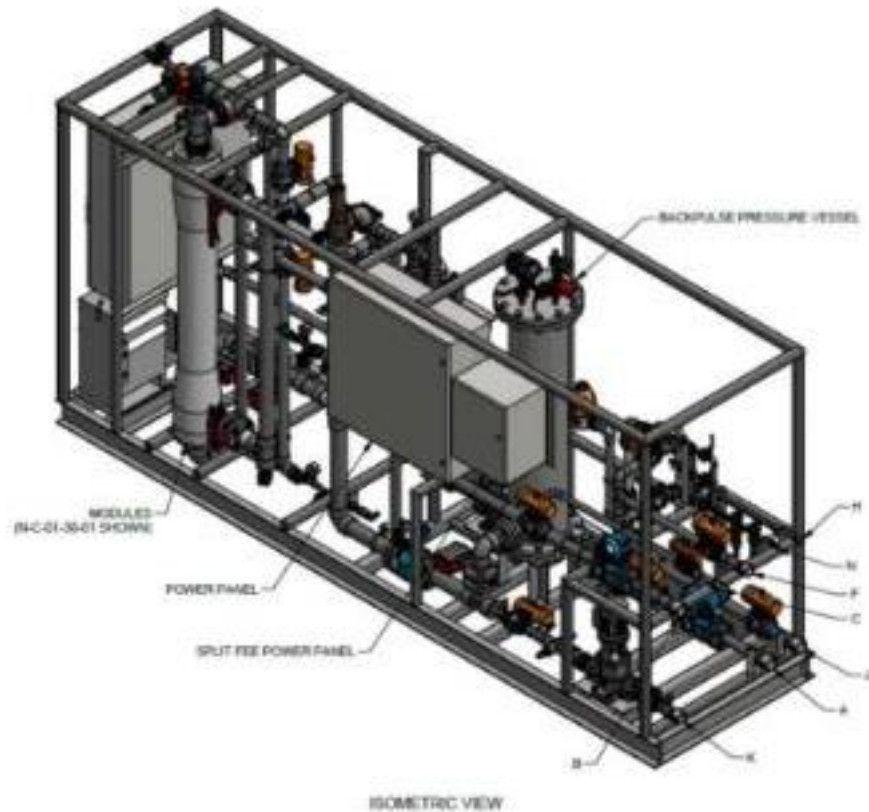
## Evaluation of Potential Advanced Membrane Technologies

- Consideration of Ceramic Options
  - “Monolithic” Ceramic Membranes
    - Flux – 150-250 gfd
    - Challenge Testing Not Yet Approved by TCEQ (potentially up to 6.5-log LRV)
    - No surface installations yet in Texas
  - “Segmented” Ceramic Membranes
    - Flux – 100-150 gfd
    - Challenge Testing Approved by TCEQ – 5.31-log LRV
    - Two full-scale surface installations in Texas

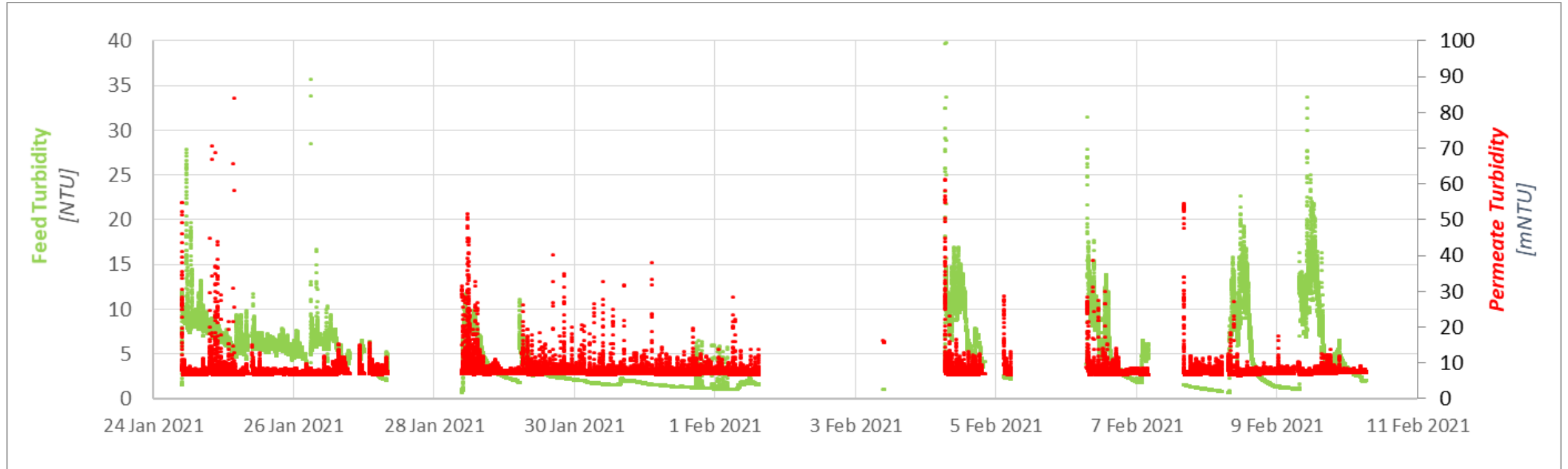




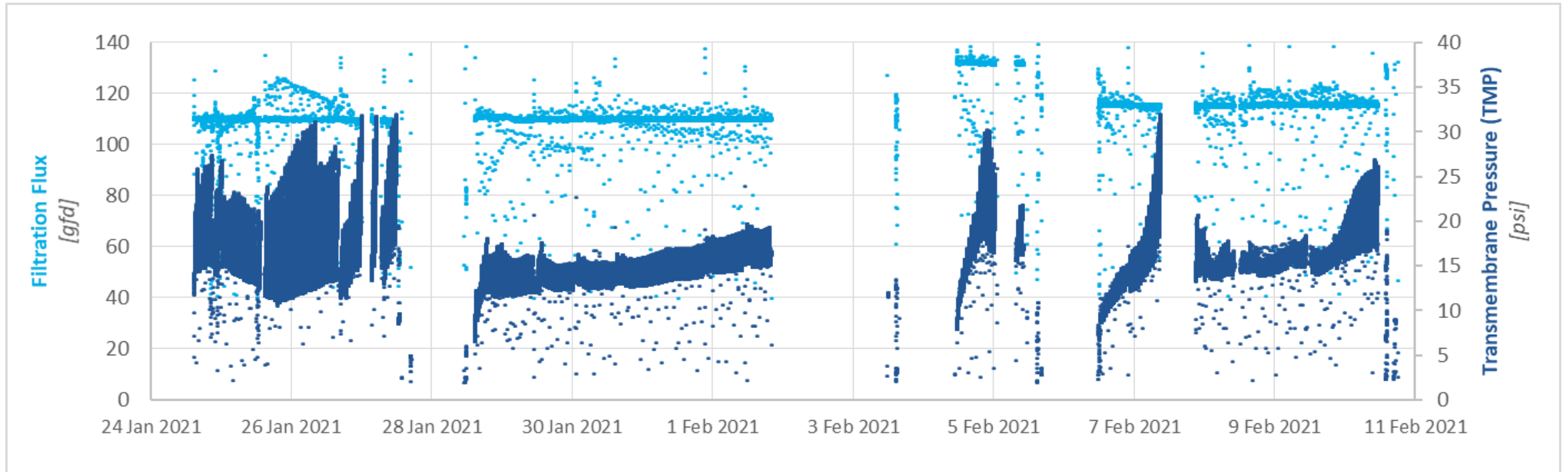
# Advanced Membrane Filter Pilot Observations



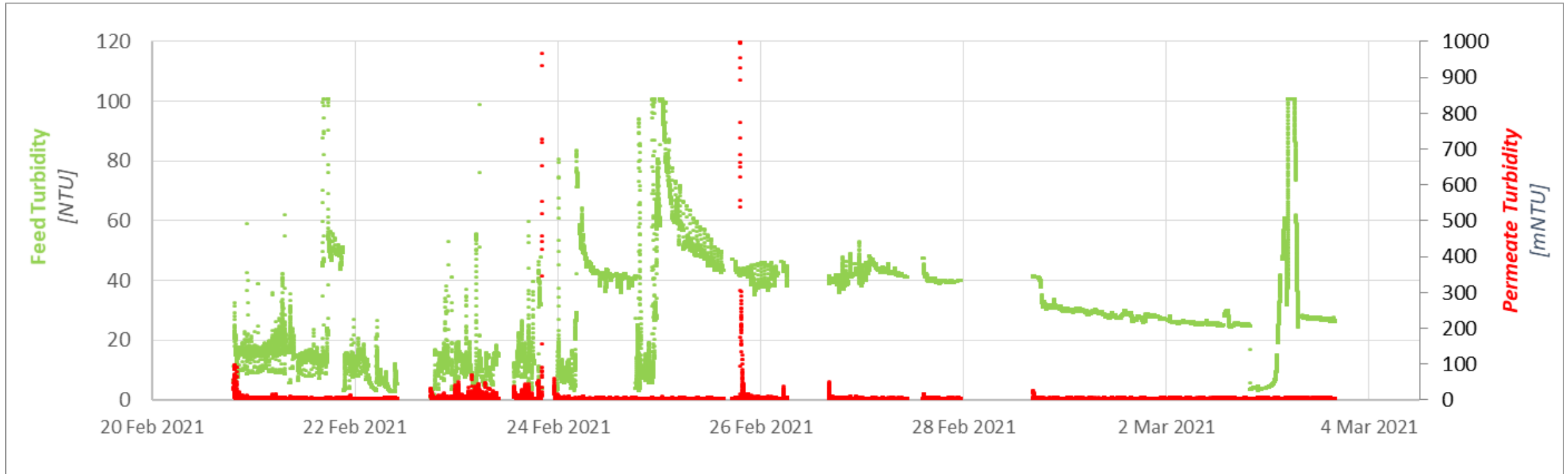
# Advanced Membrane Filter Pilot Observations



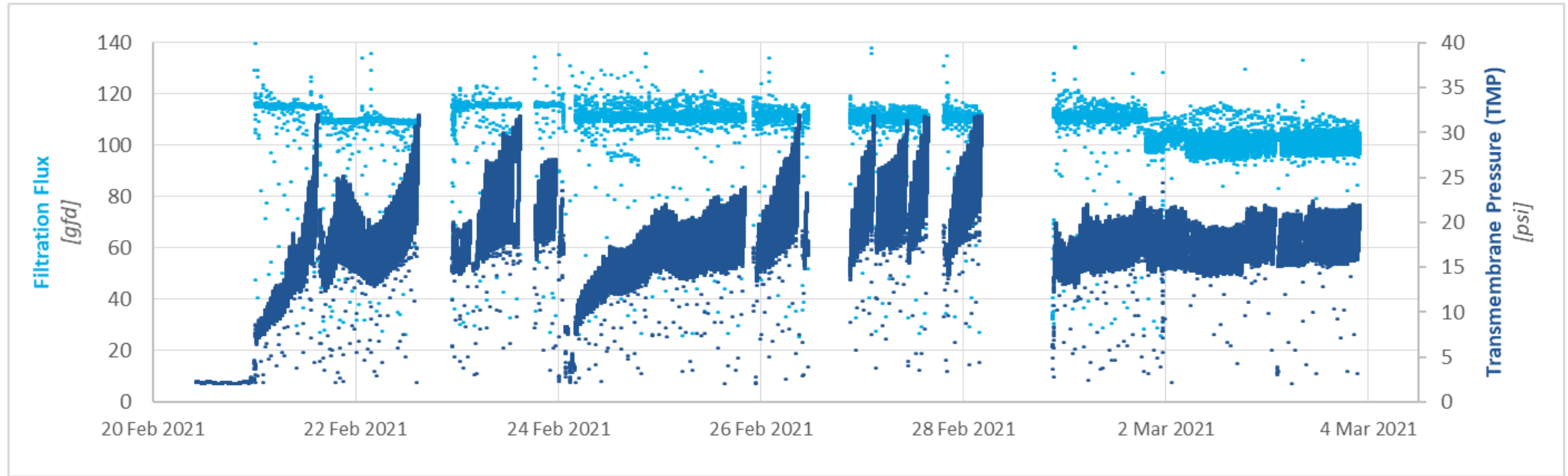
# Advanced Membrane Filter Pilot Observations



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# Advanced Membrane Filter Pilot Observations





# Advanced Membrane Filter Pilot Observations

## Final Observations

- Filtered Water Turbidity – Consistently < 0.03 NTU regardless of raw water turbidity
- Flux – Sustained at 100-115 gfd, without strong oxidant in raw water (significant colloids and organics)
  - Anticipated Future Pretreated Flux (with strong oxidant) – 125-150 gfd
- Backwash Requirements
  - Backwash rate approx. 2.5x design flow, for 30-60 second bursts
- Transmembrane Pressure (TMP) vs Feed Pressure
  - TMP range comparable to polymeric MF systems
  - Feed pressure range also comparable to polymeric MF systems

## Summary – Opportunity for Both New Systems and Retrofits

# Project Path Forward and Next Steps

- Now
  1. Coordinate with TCEQ to work toward obtaining exception approval for ceramic MF system in future Phase II WTP improvements project
  2. Implement new ClO<sub>2</sub> system, new RO Train #2, new coagulant addition, and new operational improvements as part of Phase I WTP improvements
    - Restore original 1.0 MGD WTP capacity and expand to 2.0 MGD
- Future
  1. Upgrade membrane filtration system to ceramic technology and further expand WTP to 3.0 MGD in future Phase II WTP improvements project

# Final Thoughts

- The District's original MF system could not sustain full-scale performance observed during initial 2010 pilot testing (25 gfd vs 52 gfd)
  - Even with additional modules installed, WTP could not produce the 1.0 MGD it was originally rated for
- With increasing growth in the service area, the District's WTP needs to be expanded to 2.0 MGD today, 3.0 MGD tomorrow, and even further beyond
  - The existing WTP cannot be expanded beyond 3.0 MGD if continuing to use the existing MF technology
- Pilot testing of a new segmented ceramic MF system reflected an achievable flux of 100-150 gfd, or 3-4x the capacity in the same footprint
  - A future ceramic MF system also comes with a longer full replacement membrane warranty, upwards of 20+ years

*Questions?*